

### Training-course-report: Determining Energy Efficiency of Dryers



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### **Justification**

Large-scale pneumatic dryers, used for cassava processing, have been developed over a long period of time, and are nowadays highly efficient (Sriroth et al., 2000). In contrast, small-scale dryers, are still on early stage of development and presents low energy efficiency (Precoppe et al., 2017). The objective of this training course was to strength Nigerian equipment manufacturers and service providers capacity on determining the energy efficiency of dryers.

### Methodology

The course was anchored on the constructivist learning theory (Piaget & Inhelder, 1969; Vygotsky & Cole, 1978) and knowledge was built based on the previous experiences of the participants. Learning activities included real measurements and practical calculations.

### Agenda

The training course took place in a meeting room at Green Legacy Resort, Abeokuta, Nigeria. It was done over 2 days, 18<sup>th</sup> and 19<sup>th</sup> of May 2018. The opening ceremony was conducted by Prof Lateef Sanni and had the honour presence of Prof Felix Salako, Vice-Chancellor for the Federal University of Agriculture, Abeokuta (FUNAAB), as shown on Fig 1.



Fig 1. Training course open ceremony with FUNAAB Vice-Chancellor, Prof Felix Salako.

A total of 15 engineers, composed of equipment manufacturers and service provided, attended the training course (Fig 2).





Fig 2. Equipment manufacturers and serviced providers during the training course in Abeokuta, Nigeria.

After the opening ceremony the objectives, methodology and content of the training course was presented (Appendix 1).

In the first day, measurements and efficiency calculations, were done using a domestic hair dryer. In the second day, the principles learned from the hair dryer were applied to a pneumatic dryer. Participants successfully calculated the energy efficiency of the dryer shown on Fig 3.



Fig 3. Illustration of a pneumatic dryer including data needed to determine its energy efficiency.

In the end of the training course an evaluation form was handed to the participants (Fig 4). In this hedonic scale, 1 means 'disliked extremely' and 9 means 'liked extremely'. The training course scored  $8.8 \pm 0.4$ . At the field for additional comments, all participants manifested interested on follow-up training courses (Appendix 2).

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Fig 4. Evaluation form handed in the end of the training course.

### **Subjects**

The training course was problem-centred and not content-oriented. During the practical exercises, the following subjects was explored:

- Air absolute humidity and enthalpy
- Air density and air mass flow rate
- Material moisture content
- Material mass flow rate
- Heat input rate
- Water evaporation rate
- Heat used for moisture evaporation
- Energy efficiency

A summary sheet was handed to the participants (Appendix 3) and for the calculation of the heat rate used for moisture evaporation, it was suggested to use the cassava heat of sorption instead of the latent heat of water vaporisation. This allows accounting for the energy required to overcome capillary forces bounding water molecules (Fig 5).



Fig 5. Relationship between cassava moisture content and the energy needed for water evaporation.

Participants also strengthened their knowledge on the main components of a pneumatic dryer (Appendix 4) and on properly defining system boundaries, according to objectives of the study (Fig 6).



Fig 6. Illustration of pneumatic dryers using different system boundaries, according to the objective of the study.

Finally, participants learned about the measurements and data collection needed to determine energy efficiency of pneumatic dryer (Fig 7).



Fig 7. Measuring protocol to determine energy efficiency of a pneumatic dryer.

### Outcome

Equipment manufacturers and service providers strengthened their knowledge on determining the energy efficiency of dryers. They all stated that trainings like this are very important and beneficial. All of participants expressed interest on following-up training courses. Two main topics were requested: (a) advance training on energy performance evaluation of dryers; (b) properly designing and dimensioning a pneumatic dryer. It has also been discussed about creating an online forum using CassavaTech.com platform. The forum would allow them to exchange their calculations and experiences on the topic.

### References

Piaget, J., & Inhelder, B. (1969). The Psychology of the Child. New York, NY: Basic Books.

- Precoppe, M., Chapuis, A., Müller, J., & Abass, A. (2017). Tunnel Dryer and Pneumatic Dryer Performance Evaluation to Improve Small-Scale Cassava Processing in Tanzania. *Journal of Food Process Engineering*, 40.
- Sriroth, K., Piyachomkwan, K., Wanlapatit, S., & Oates, C. G. (2000). Cassava starch technology: The Thai experience. *Starch Stärke*, 52, 439–449.
- Vygotsky, L. S., & Cole, M. (1978). *Mind in Society: Development of Higher Psychological Processes*. Cambridge, MA: Harvard University Press.







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# Welcome to the course

Determining energy efficiency of dryers



NRI | Natural Resources Institute



• Learn to determine the energy efficiency of dryers

2

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# Method

- Two-days intensive-course
- Hands-on
- No lectures
- No PowerPoint
- No training material
- No certification of conclusion



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3

What is	s your	overall	opinion	about	this	training	course?	
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7

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## Determining energy efficiency of dryers

A two-days intensive-course facilitated by Dr Marcelo Precoppe Crop Postharvest Technologist | Food and Markets Department | Natural Resources Institute | Faculty of Engineering and Science | University of Greenwich

#### Absolute humidity (gwater kgdry air<sup>-1</sup>)

The absolute humidity (Y) can be calculated from measured values of temperature (T) relative humidity ( $\varphi$ ) and pressure (P).

#### Air enthalpy (kJ kg<sub>dry air</sub><sup>-1</sup>)

Enthalpy of the air (h) can be calculated from measured values of temperature (T) relative humidity ( $\varphi$ ) and pressure (P).

#### Solid moisture content on a dry basis (kg<sub>water</sub> kg<sub>dm</sub><sup>-1</sup>)

Solid moisture content on a dry basis (X) is measured at the lab, most commonly using the oven method.

#### Solid mass flow rate on a dry basis (kg<sub>dm</sub> h<sup>-1</sup>)

The solid mass flow rate on a dry basis ( $\dot{m}_{dm}$ ) is calculated from dried solid output rate ( $\dot{m}_{ds}$ ) and the dried solid moisture content ( $MC_{ds}$  or  $X_{ds}$ ).

#### Air density (kg m<sup>-3</sup>)

Density of the air  $(\phi)$  is calculated from measured values of temperature (*T*) relative humidity  $(\phi)$  and pressure (*P*) Calculated from air temperature relative humidity and pressure.

#### Air mass flow rate on dry basis (kg<sub>dry air</sub> h<sup>-1</sup>)

Air mass flow rate ( $\dot{m}_{air}$ ) measured air velocity and cross-sectional area plus the calculated is calculated air density ( $\rho$ ).

#### Heat input rate to the dryer (kW or MJ h<sup>-1</sup>)

Heat input rate ( $\dot{Q}_{in}$ ) is the energy provided to the dyrer, and is calculated as shown:

$$\dot{Q}_{\rm in} = \dot{m}_{\rm air} \cdot h_{\rm in}$$

Where  $m_{air}$  is the air mass flow rate,  $h_{in}$  is the enthalpy of the air at the dryer inlet and  $h_{amb}$  is the enthalpy of the ambient air.

#### Water evaporation rate (kg<sub>water</sub> h<sup>-1</sup>)

The water evaporation rate ( $\dot{m}_{w}$ ) is calculated based on the solid mass flow rate on a dry basis ( $\dot{m}_{dm}$ ) and the difference between the wet solid moisture content on a dry basis ( $X_{ws}$ ) and the dried solid moisture content on a dry basis ( $X_{ds}$ ):

$$\dot{m}_{\rm w} = \dot{m}_{\rm dm} \left( X_{\rm ws} - X_{\rm ds} \right)$$

#### Heat rate used for moisture evaporation (MJ h<sup>-1</sup>)

Heat rate used for moisture evaporation  $(\hat{Q}_w)$  is obtained by multiplying the water evaporation rate  $(\hat{m}_w)$  with the latent heat of water vaporisation  $(\lambda)$ :

$$Q_{\rm w} = \dot{m}_{\rm w} \cdot \lambda$$

#### **Energy efficiency (%)**

Energy efficiency ( $\eta$ ) is the ratio between the heat rate used for moisture evaporation ( $\dot{Q}_{w}$ ) and the heat rate supplied to the dryer ( $\dot{Q}_{m}$ ):

$$\eta = \frac{Q_{\rm w}}{\dot{Q}_{\rm in}}$$













