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2 **Sensitivity analysis of deep geothermal reservoir:**  
3 **effect of reservoir parameters on production temperature**  
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10  
11 **Abstract**

12 This study aims to guide reservoir engineers/managers in the selection of a combination of  
13 parameters from amongst various possible alternatives in developing deep geothermal  
14 reservoirs which can meet the desired temperature at the production wellhead for sustainable  
15 energy production. The work presents an approach for predicting the long-term performance  
16 of a deep geothermal reservoir using multiple combinations of various reservoir parameters.  
17 The finite element method and factorial experimental design are applied to forecast which of  
18 the parameters has the most influence on long-term reservoir productivity. The solver  
19 employed is validated using known analytical solution and experimental measurements with  
20 good agreement. After the validation, an investigation is then performed based on the Soultz  
21 lower geothermal reservoir. The results showed that fluid injection temperature is the parameter  
22 that influences the experiment the most during exploitation involving production temperature,  
23 whereas injection pressure rate happens to have a more significant impact on reservoir cooling.  
24

25  
26 **Keywords:** Deep geothermal reservoir; human-controlled parameters; naturally-occurring  
27 parameters; finite element modelling; factorial experimental design.  
28

29 **1. Introduction**

30 Geothermal energy production is, and for the predictable future will remain, one of the most  
31 important activities that can provide a solution to the current clean and sustainable energy  
32 demand in the world. The objective is to discover and produce energy located at a great depth  
33 in an efficient way by applying a synergy of various scientific disciplines (geology, geophysics,  
34 seismology, and reservoir engineering). In a deep geothermal system, reservoir rock parameters  
35 determine the value of accumulated heat and energy[1]. Their quantity and productivity also  
36 ascertain the value of the accumulated energy. In reservoir management, both production rate  
37 and producibility are functions of the rock and reservoir fluid parameters [2]. For example, the  
38 capacity of a well depends on rock parameters (permeability, porosity, reservoir thickness), on  
39 fluid properties (density, viscosity), on the well type (vertical, horizontal), and on the pressure  
40 drop applied at the bottom hole. Also, the productivity of a geothermal well depends, among  
41 other things, upon the permeability of reservoir formation to those fluids, and anything that  
42 increases the permeability of the formation will increase the rate of energy production.  
43 Injection fluid in geothermal energy exploitation is one of the most important parameters that  
44 can be controlled during operations. This is because the fluid is heated to a precise temperature  
45 before injection. Mostly, after extracting the fluid back for usage, it is then transferred to a  
46 cooling tower for reinjection/reuse. The wellhead pressure and its relation to the flow rate of  
47 fluid via the turbine is an additional parameter that must be considered when generating power  
48 from geothermal resources. Likewise, the well spacing is decided by an ease of drilling and  
49 also by the evidence that the geothermal resource enclosed by the well pattern must be extracted  
50 during an economically acceptable period of 30 years [3]. This factor is determined by the fluid  
51 properties, the well capacity, the reservoir parameters, and distribution. If the exploitation of a  
52 geothermal reservoir takes place by so-called enhanced geothermal system (EGS) methods (as  
53 in this study), the well spacing is significantly less than in the case of production via the primary  
54 method [4].

55 Therefore, the interaction of this parameter with others can provide deeper insight into  
56 reservoir management. For instance, permeability is one of the fundamental parameters of a  
57 reservoir that controls the fluid flow in a deep geological formation. Reservoir stimulation  
58 increases the permeability of a system due to stress perturbation taking place as exploitation  
59 proceeds. However, coupled hydro-thermal analyses is not a candidate to capture the effect of  
60 such changes in permeability when simulating, though varying the values can provide a close  
61 solution to the real life scenario. On the other hand, porosity is another parameter that  
62 contributes in enhancing reservoir productivity because it concerns the volume fraction of the

63 rock matrix to the pore space [5]. It is tough to estimate the porosity values for an entire matrix  
64 block in deep reservoirs due specifically to the limitations of the current measuring techniques  
65 [6]. Thus, it is expected to range the porosity values and examine their effect on reservoir  
66 productivity. Thermal conductivity, on the other hand, signifies the ability of material to  
67 transfer heat [7]. In deep subsurface systems, the value of the thermal conductivity of a  
68 formation is dependent on temperature, pressure, and porosity [8].

69 It is observed from the literature [9]–[14] that, as far as the application of finite element  
70 heat transfer and fluid flow problems to geothermal energy are concerned, a lot of studies are  
71 available. However, no study appears to be available that deals with multiple parameter  
72 interactions in geothermal energy exploitation. Based on this, the objective of the present study  
73 is to explore the possible combination of critical parameters in a deep geothermal reservoir that  
74 can meet a certain production temperature requirement during a long-term simulation of 60  
75 years. The work identifies two group of parameters, which are human-controlled and naturally-  
76 occurring parameters, and their interactions provide preliminary indications of the potential  
77 productivity of a geothermal reservoir. A three-dimensional (3-D) model of the Soultz (France)  
78 deep geothermal reservoir is developed on COMSOL FE package, which is a commercial  
79 software that allows the implementation of user-defined subroutines from the MATLAB  
80 programming language in the simulation. The package is widely employed in industries and  
81 institutions for its capability to accommodate extensive material modelling and the coupling of  
82 several systems in finite element analyses. Before running the analysis, the numerical code is  
83 validated first with known analytical solution and experimental measurements to ascertain the  
84 capability of the chosen simulator. In the reservoir analysis, the required temperature fields are  
85 calculated by solving a forward problem using the finite element method. For predicting the  
86 possible combinations, a complete factorial experimental design is chosen for the analyses.

87 In this study, the sensitivity analysis is limited to the maximum and minimum values  
88 of the reservoir parameters analysed. Knowing the influence of a certain parameter under a  
89 minimum or maximum value when combined with other parameters will provide an  
90 understanding of which of the values is significant. Besides, it reduces the computational cost  
91 without compromising the outcome of the analysis. For example, lateral well spacing, as a  
92 human-controlled parameter when narrowly spaced, will likely result in short-circuiting,  
93 whereas wider spacing makes it harder to establish a connection between the wells. Therefore,  
94 careful considerations have to made when selecting the minimum or maximum value of the  
95 reservoir parameters. The various parameters are taken from the general engineering  
96 observation's point of view in the real field case for the Soultz geothermal reservoir.

97

## 98 **2. Mathematical background**

99 The finite-element method is used for solving the macroscopic transient coupled equations of  
100 heat transfer and fluid flow in a fully saturated and fractured porous medium as implemented  
101 in the forward modelling code chosen. Thus, the dual porosity-permeability approach is  
102 employed in solving the macroscopic partial differential equations (PDE's) for both the matrix  
103 and fracture systems. In this approach, the rock matrix is considered to have high porosity and  
104 low permeability, while the fracture, on the contrary, has low porosity and high permeability.  
105 The irregular fracture system crossing the matrix provides perhaps the recovery of the  
106 accumulated heat and energy.

107

### 108 **2.1 Governing equations**

109 The macroscopic equations describing heat and fluid transport in fractured and saturated porous  
110 media can be numerically investigated by coupling the appropriate rock and fluid physical  
111 properties, respectively. For the heat transport, the transfer in porous matrix is governed by  
112 both conduction and convection [15], which is written as

$$113 \quad \rho C_p \frac{\partial T}{\partial t} + \rho_L C_{p,L} v \cdot \nabla T - \nabla(\lambda \cdot \nabla T) = 0 \quad (1)$$

114 where  $\rho$  and  $C_p$  are the effective densities and specific heat capacities, respectively,  $T$  is the  
115 temperature, and  $t$  is time. Properties,  $\rho_L$  and  $C_{p,L}$  corresponds to fluid density and specific  
116 heat capacity,  $v$  is Darcy's velocity and  $\lambda$  is the effective thermal conductivities. The  
117 properties of the porous media obey a simple mixing rule between solid (S) and liquid (L),  
118 expressed as

$$119 \quad \rho C_p = \phi(\rho_L C_{p,L}) + (1 - \phi)\rho_S C_{p,S} \quad (2)$$

$$120 \quad \lambda = \phi(\lambda_L) + (1 - \phi)\lambda_S \quad (3)$$

121 here  $\phi$  is the porosity and  $\rho_S$  is the solid density. Properties,  $\lambda_L$  and  $\lambda_S$  are the fluid and solid  
122 thermal conductivities, respectively.

123

124 For the fluid flow within a matrix block [16], the equation writes

$$125 \quad \rho_L S \frac{\partial P}{\partial t} + \nabla \cdot \rho_L v = 0 \quad (4)$$

126 where  $S$  is the linearised storage, and  $P$  is the fluid pressure, and Darcy's velocity  $v$  is written  
 127 as

$$128 \quad v = -\frac{\kappa}{\mu}(\nabla P - \rho_L g \nabla z) \quad (5)$$

129 here  $\kappa$  is the permeability,  $\mu$  is the fluid viscosity,  $g$  is the acceleration due to gravity and  $z$   
 130 is the depth.

131

132 Similarly, the heat transport in fractures within a porous matrix is given by

$$133 \quad \rho C_P \frac{\partial T}{\partial t} + \rho_L C_{P,L} v_f \cdot \nabla T - \nabla(\lambda \cdot \nabla T) + Q_{f,E} + Q_{m,E} = 0 \quad (6)$$

134 parameters,  $Q_{f,E}$  and  $Q_{m,E}$  corresponds to the energy sources/sinks for the fracture and matrix  
 135 block. The fracture Darcy's velocity term  $v_f$  is expressed as

$$136 \quad v_f = -\frac{b^2}{12\mu}(\nabla P_f - \rho_L g \nabla z) \quad (7)$$

137 where  $b$  is the fracture aperture, and  $P_f$  is the fluid pressure within the fracture. The fluid flow  
 138 within the fracture is written as

$$139 \quad \rho_L S_f \frac{\partial P_f}{\partial t} + \nabla \cdot \rho_L v_f + Q_f + Q_m = 0 \quad (8)$$

140 where  $Q_f$  and  $Q_m$  are the fluid mass sources/sinks for the fracture and matrix block and  $S_f$  is  
 141 the fracture storativity.

142

143 Coupling between the fluid motion and heat transport is carried out through  $\rho_L$ ,  $\mu$ ,  $C_{P,L}$ , and  
 144  $\lambda_L$  parameters that appear in almost all the Equations (1) - (8), which are coupled by the  
 145 temperature field (T), since all the properties are temperature-dependent, which will be  
 146 discussed later. Also, the coupling between heat transport and fluid flow is achieved through  
 147 Darcy's velocity term (contribution of convective heat transfer) that appears in Equations (1),  
 148 (4), and (5) for the matrix block, and (6), (7) and (8) for the fracture.

149

## 150 **2.2 Fluid and rock physical properties**

151 In this study, the fluid properties are assumed to vary with temperature. For the fluid density  
 152 in kg/m<sup>3</sup>, the fitting polynomial trend proposed by Holzbecher [17] has been chosen, and is  
 153 written as

$$154 \quad \rho_L(T) = 996.9 \left( 1 - 3.17 \times 10^{-4} (T - 298.15) - 2.56 \times 10^{-6} (T - 298.15)^2 \right) \quad (9)$$

155 The temperature in equation (9), ranges from 20°C to 250°C. The analytical expression adopted  
 156 for the relationship between dynamic viscosity in Pa·s and temperature [18] given as

$$157 \quad \mu(T) = 2.414 \times 10^{-5} \times 10^{\frac{247.8}{(T+133)}} \quad (10)$$

158 In equation (10) the temperature ranges between 4 and 250°C. For the thermal conductivity in  
 159 10<sup>3</sup> W/m/K, the following fitting polynomial is employed [3]

$$160 \quad \lambda_L(T) = -922.47 + 2839.5 \left( \frac{T}{T_0} \right) - 1800.7 \left( \frac{T}{T_0} \right)^2 + 525.77 \left( \frac{T}{T_0} \right)^3 - 73.44 \left( \frac{T}{T_0} \right)^4 \quad (11)$$

161 where  $T_0$  is 273.15 K, and the temperature ranges between 0°C and 350°C, and according to  
 162 Holzbecher [17], specific heat capacity of fluid at temperatures between 100°C and 320°C can  
 163 be approximated by

$$164 \quad C_{p,L}(T) = 3.3774 - 1.12665 \times 10^{-2} T + 1.34687 \times 10^{-5} T^2 \quad (12)$$

165 The unit of equation (11) is [cal/g/K], to obtain the SI units [J/kg/K] it has to be multiplied by  
 166 4187.6. Specific heat capacity below the temperature of 100°C seems to be constant with a  
 167 value of 4200 J/kg/K approximately [17].

168

### 169 **3. Validations**

170 Before proceeding with the investigation, it is required to be first convinced that the numerical  
 171 solutions are valid. The typical method of validating a numerical solution is to use a simple  
 172 problem for which analytical solutions are available and, after that, to test the numerical  
 173 solution with the chosen analytical solution. One of the main issues of this method is that it can  
 174 only be employed in extremely simple problems because seeking to obtain the analytical  
 175 solution of real problems is practically impossible. Apart from analytical solutions, the most  
 176 common method used in validating a numerical simulation is through experimental  
 177 measurements. This method is more reliable due to the fact that measurements show the  
 178 consistency of the solution in reality. Thus, it is important to note that when an experiment is

179 performed, a measuring instrument must be introduced; once employed, it directly or indirectly  
 180 affects the system being measured. However, at the end of the validation process, it is crucial  
 181 to have the greatest similarity between the measurement and numerical simulation.

182 Therefore, in this study, both the analytical and experimental measurements are  
 183 employed in validating the numerical simulation chosen in this research as presented in the  
 184 upcoming sections.

185

### 186 **3.1 Numerical validation of analytical solution**

187 The validation of the analytical model is based on heat diffusion and advection through a rock  
 188 matrix orthogonal to a fracture, as shown in Fig. 1. Coupling of the advective 1D heat transport  
 189 in the fracture and diffusive 1D heat transport in the rock matrix is also presented in the  
 190 analytical solution. Thus, the rock matrix elements are linked to the fracture elements  
 191 orthogonally, which implies that the nodes in the matrix are not influenced by their right or left  
 192 boundaries. In the present study, the analytical solution, often referred to as Lauwerier's  
 193 Solution, is examined and compared with numerical results concerning the temperature  
 194 breakthrough curves at certain positions within the rock matrix. The analytical solution is  
 195 derived based on the assumptions that heat is transferred only by advection in the fracture, and  
 196 also, heat transfer takes place by diffusion in the rock matrix along the z-axis only [19]. Thus,  
 197 the Lauwerier's solution is given by

$$198 \quad T = \begin{cases} 0, & t_D < x_D \\ \operatorname{erfc} \left\{ \frac{\beta}{\sqrt{\alpha(t_D - x_D)}} \left[ x_D + \frac{1}{2\beta} \left( z_D - \frac{1}{2} \right) \right] \right\}, & t_D > x_D, z_D \geq \frac{1}{2} \end{cases} \quad (13)$$

199 where the following parameters from equation (13) are dimensionless:

$$200 \quad t_D = \frac{vt}{b_w}, \quad x_D = \frac{x}{b_w}, \quad z_D = \frac{z}{b_w}, \quad \alpha = \frac{\lambda_s}{C_{p,S} \rho_S} \frac{1}{b_w v}, \quad \beta = \frac{\lambda_s}{C_{p,L} \rho_L} \frac{1}{b_w v} \quad (14)$$

201 where  $v$  is the groundwater velocity,  $b_w$  is the fracture width, while  $x$  and  $z$  represents the  
 202 dimensions of the axes.

203 Table 1 presents the model and material parameters employed in the study [19]. Fig. 2  
 204 shows the schematic description of the model and the relevant boundary conditions, but due to  
 205 symmetry, only the domain above the x-axis is considered in the numerical investigations. Fig.  
 206 3 presents the locations of specific points chosen to observe the temperature breakthrough  
 207 curves in order to assess the numerical simulation in comparison with the analytical solutions.

208 Fig. 4 shows the numerical simulation results, compared to the analytical solution at  
209 the three chosen points on the rock matrix. The plotted temperature breakthrough curves and  
210 the time are both considered to be dimensionless parameters. At the observed points, it can be  
211 seen that there are slight differences between the numerical results and the analytical solutions,  
212 but after some time, both solutions fit very well. The cause for the slight deviation between the  
213 analytical solution from the numerical results is because at the early simulation period (200  
214 and 400), the breakthrough temperature of the numerical model points far from the fractures  
215 are not affected by the fluxes at the fracture's edge due to different modelling assumptions of  
216 fracture flow. The analytical model assumed the fracture to be an equivalent porous medium  
217 whereas the numerical model used the cubic law of parallel plates. However, after a longer  
218 period of simulation (600, 800, and 1000), both results fit very well together.

219 In addition, another possible reason for the primary difference may likely be due to the  
220 inclusion of a viscosity parameter in the numerical simulations, which is not present in the  
221 analytical solution. In summary, it is concluded that both the numerical simulation and  
222 analytical solution are in good agreement.

223

224

### 225 **3.2 Validation of temperature profile at Soultz well**

226 In line to carry out a validation study on a geothermal system, the lower granite of the Soultz  
227 geothermal system is chosen due to the situation of the lower reservoir within this vicinity.  
228 Thus, validation of the temperature profile of this lower section of the system is paramount in  
229 justifying the validity of the proposed model. A steady-state simulation is carried out on the  
230 Soultz geothermal system to validate the proposed model by predicting the temperature profile  
231 variation with depth. The measured temperature profile at Soultz wells are reported in works  
232 of literature [20], [21]. The predicted temperature profile proposed at a depth of the lower  
233 granite in Soultz (i.e., 3.5 km to 5.4 km) is compared to the recorded data obtained at well  
234 GPK2 for the Soultz geothermal system. As shown in Fig. 5, the experimental and simulated  
235 temperature profiles show a typical trend pattern with increasing magnitude with depth. The  
236 overall agreement is reasonably sound with some slight differences at certain depths.

237 Table 2 presents the percentage difference between the measured and simulated  
238 temperature profile at well GPK2. As seen, from the depths observed, the maximum deviation  
239 is 3.19%, and the minimum difference is 0%. These differences in temperature profile could  
240 be attributed to the following reasons. (1) Both Heat and fluid flow are modelled at steady state;  
241 therefore, energy loss due to the acceleration of fluid is not accounted. (2) Non-uniform fluid



242 properties and geological formations having different thermal properties may likely influence  
243 the deviations between the results. (3) Other possible effects such as chemical and mechanical  
244 interactions presented during the measurements are not captured in the simulations.

245 It is also important to note that only measured values of the density, porosity, and  
246 permeability from the sample cores obtained from the wellbores are employed as inputs to this  
247 model.

248

#### 249 **4. Case study: Soultz geothermal reservoir**

250 The interest generated by the Fenton Hill geothermal project resulted in several experimental  
251 studies in the European countries (the United Kingdom, Germany, and France), and due  
252 specifically to the high cost of large-scale experiments, an agreement was reached by the  
253 European countries to pool both financial and manpower resources on a single site with the  
254 aim to develop a commercial demonstration project within Europe [22]. The European  
255 Commission coordinated the selection of the most suitable of the three major sites  
256 (Rosemanowes, Soultz, and Bad Urach) and decided to locate the project to Soultz in 1987.  
257 The European Commission initially funded the project with the help of relevant energy  
258 ministries from France, the United Kingdom, and Germany [23]–[25]. The Soultz project is  
259 developed in three major stages: the preliminary stage (1984-1987), the drilling and exploration  
260 stage (1987-2007), and the power plant construction stage (2007-2008) [26]. However, the goal  
261 of this study is to model the lower geothermal reservoir, which happens to fall during the  
262 second stage of the project. Fig. 6 showed the schematic diagram of the Soultz triplet  
263 geothermal system [27]. As can be seen, the wells are drilled from the same platform on the  
264 surface, with a lateral distance of 6 m between each well. On the other hand, at the bottom hole,  
265 the lateral distance between each of the production wells from the injection well is 0.6 km [28].  
266 The wells are fully cased from the surface down to the top of the lower reservoir level (4.5 km),  
267 whereas there is an open hole section of about 0.5 km in length from the starting point of the  
268 lower reservoir, with an 8.5-inch diameter [29]. Regarding fractures, three categories exist  
269 within the lower reservoir, ranging from active to non-active [30], [31], but here, only one  
270 active fracture is considered.

271

#### 272 **4.1 Geometrical and physical properties of the reservoir**

273 An ideal numerical model of the lower reservoir has been developed to simplify the  
274 calculations, as shown in Fig. 7. In order to investigate the physical variation such as pressure  
275 and temperature in the rock matrix induced as a result of extraction processes from the hot dry

276 rock (HDR); it is significant to understand the changes of the physical features, not only amid  
277 the fracture but also between the rock matrix and the fracture, simultaneously. In achieving  
278 these goals, a fracture is introduced in the model to clarify the physical model and reduce the  
279 computational workload. The fracture intersects at a depth of 4.77 km, the coordinates of the  
280 fracture (0.15-1.8 km, 0.25 km, 4.5-5.1 km) with an inclined angle of 60°. The injection well  
281 GPK3, in the lower reservoir, is at coordinates (1 km, 0.25 km, 4.5-5.1 km); the coordinates of  
282 the first production well GPK2 are (1.5 km, 0.25 km, 4.5-5 km) with an inclination angle of  
283 10°. The coordinates for the second production well GPK4 (0.5 km, 0.25 km, 4.5-5.1 km) have  
284 an inclination angle of -10°.

285 For the rock petrophysical properties (thermal conductivity, density, porosity,  
286 permeability and heat capacity) of the Soultz (France) lower geothermal reservoir (4.5-5.0 km)  
287 are taken from literature and previous hypotheses [15], [32], [33], and are provided in Table 3.  
288

#### 289 **4.2 Initial and boundary conditions**

290 The temperature profile of the Soultz geothermal system possesses a dynamic gradient trend.  
291 The upper formation (i.e. 0–1.0 km) holds a gradient of 110°C/km, whereas the intermediate  
292 (i.e. 1–3.5 km) and lower formations (i.e. 3.5–5.3 km) possess gradients of 5°C/km and  
293 30°C/km, respectively [34]. Given that this study is concerned with lower reservoir modeling  
294 with a bottom hole temperature of 200°C, to achieve the targeted bottom hole temperature in  
295 the lower reservoir, a gradient of 38°C/km is adopted for the investigations. The initial  
296 temperature is expressed as

$$297 \quad T_0(z) = 12^\circ\text{C} - 38^\circ\text{C}/\text{km} \times (-z) \quad (15)$$

298 where  $T_0(z)$  is the initial temperature of the reservoir,  $12^\circ\text{C}$  is the assumed value of the  
299 surface temperature,  $38^\circ\text{C}/\text{km}$  is the geothermal gradient, and  $z$  is depth in kilometres. The  
300 initial pressure is assumed to be hydrostatic throughout the reservoir.

301 A Dirichlet boundary condition (BC) of 30°C (injection temperature) is applied as a  
302 thermal boundary condition, whereas for the hydraulic case, 10 MPa (injection pressure) was  
303 considered as the Dirichlet BC on the wellbore injection GPK3. On the other hand, an  
304 underpressure BC of -10 MPa is employed on both the production wells GPK2 and GPK4,  
305 individually. All other boundaries remain insulated during simulations.

306

#### 307 **4.3 Meshing and solutions**

308 To obtain a reliable finite element solution, a well-defined meshing technique is required. In  
309 particular, in deep reservoir modelling, several structures are considered with highly varying  
310 scales. For example, in the interaction between reservoir wells and rock matrix, the former is  
311 in millimetres, whereas the latter is in thousand meters or kilometres. Thus, meshing structures  
312 of this kind necessitate a special approach. In this study, isoparametric elements are chosen for  
313 meshing the various reservoir components. A four-node tetrahedral element is adopted for the  
314 discrete of the matrix, a three-node triangular element for the fractures, and a two-node line  
315 element for the wells. Extremely fine, extra fine, and finer grids are employed to scatter  
316 computation vicinity. The major complexity of this meshing approach lies in maintaining the  
317 internal geometric uniformity between well, fracture, and matrix elements.

318 In Fig. 8, finer grids of moderate element size scatter the matrix domain and its  
319 boundaries far away from the fracture and the wellbores, whereas extra fine grids are created  
320 within the fracture and the neighbouring matrix attached to it. For the wellbores, extremely fine  
321 grids are employed by regulating the element growth rate between the wellbores, fracture, as  
322 well as the rock matrix, as shown in Fig. 8. Fig. 8 also presents the element size distribution of  
323 the reservoir model. As can be seen in the figure, the minimum element size is 0.14 m, and the  
324 maximum size is 84.6 m. The distribution depends on a structural dimension; for example, the  
325 wellbore that has the slender dimension and the elements within its region are smaller in size  
326 in comparison to the fracture and matrix elements. The mesh generated results in 966,213  
327 tetrahedrons, 41,904 triangulars, 3,272 edges, and 58 vertex elements. The mesh division  
328 approach improves the calculation precision and also eliminates the deviation rate induced by  
329 unsuitable selected boundary conditions.

330 The simulation is run for 60 years, and because of the long simulation time and the  
331 stability provided by the constant temperature and pressure conditions, a backwards difference  
332 formula (BDF) is employed in the COMSOL package. The scheme holds an advantage of  
333 limiting time step. In the present study, it took only 47 time steps to simulate the 60-year  
334 experimentation. The physical memory used for the simulation is 3750 MB, and the virtual  
335 memory is 3980 MB.

336

## 337 **5. Results and Discussions**

338 After successful completion of the validation studies, this study seeks to identify some response  
339 parameters that govern the behaviour of geothermal reservoirs subjected to different  
340 operational conditions, as well as to assess their long-term performance. The proposed  
341 methodology consists of using a 3-D model of the Soultz lower geothermal reservoir to

342 comprehend the result of interactions between several independent parameters in geothermal  
343 energy exploitations by employing a complete factorial experimental design.

344 In predicting a possible combination, the value ranges for various reservoir parameters  
345 are chosen based on previous field experiments conducted at Fenton Hill (US), Rosemanowes  
346 (UK), Hijori and Ogachi (Japan), and Soultz (France) geothermal projects. These can all be  
347 found in the MIT report [22]. For instance, it is known from field experience that thermal  
348 conductivity of most of the rocks falls within 1.0 to 3.5 W/m/K. Similarly, for porosity, the  
349 same has also been assumed to lie between 10% to 40% for most formations. In a similar  
350 context, different value ranges are prescribed for rock permeability (0.1 mD - 0.01 mD) and  
351 geothermal gradient (28°C/km - 38°C/km).

352 In the case of human-controlled parameters, the injection pressure selection depends on  
353 the value of measured minimum principal stress to create hydraulic fractures. In this study, the  
354 choice of maximum and minimum injection pressure (10 MPa - 25 MPa) is based on the Soultz  
355 and Fenton Hill projects, respectively. Similarly, for injection temperature, the values gathered  
356 for most reservoirs lie between 30°C and 60°C. Also, different value ranges are prescribed for  
357 the injection flow rate (10 l/s - 70 l/s), and lateral well spacing (0.3 km - 0.6 km).

358 Table 4 presents the human-controlled parameters chosen for the studies, for each of  
359 the parameters the values ranges from minimum to maximum as mentioned above. Thus, two  
360 values are assigned to each individual parameter and all the possible combinations of other  
361 parameters in the same group are evaluated. The number of runs required for each group is  $2^n$ ;  
362 this identifies the number of parameters ( $n$ ), how many levels each parameter has (2), and how  
363 many experimental conditions there are in the design ( $2^n$ ). Each independent parameter is a  
364 factor in the design because there are four parameters and each parameter has two levels of  
365 factorial design in each group.

366 Similarly, Table 5 presents the naturally occurring parameters with their minimum and  
367 maximum values using the same factorial experimentations design as in the human controlled  
368 parameters. Thus, this studies will have  $2^n = 16$  different experimental conditions for each of  
369 the human-controlled parameters, and naturally-occurring parameters as presented in Tables 6  
370 and 7.

371 It is worthy to mention that, the temperature in the production wellbores GPK2 and  
372 GPK4 are found to be identical in all cases. Thus, for clarity purposes, only the simulation  
373 results obtained in production wellbore GPK2 are presented here.

374

## 375 **5.1 The effect of human-controlled parameters on production temperature**

376 A complete factorial experimental design is used in implementing the possible combinations  
377 required, and for this case, it results to 16 different operational scenarios as shown in Table 6.  
378 The studies involve understanding the effect of various interactions of these parameters on  
379 reservoir productivity. Fig. 9a showed the production temperature history at wellhead GPK2,  
380 during the long-term simulation of 60 years for the Soultz lower reservoir, under the influence  
381 of multiple parameter interactions for the human-controlled parameters. Four interaction  
382 scenarios are considered by varying the injection temperatures and pressures while keeping the  
383 injection rate (10 l/s) and lateral well spacing (0.3 km) at a constant rate. As can be seen, lower  
384 injection temperature, when interacting with lower injection pressure, yields maximum  
385 production temperatures at the wellhead. The reason for that is the propagation of cold water  
386 is much slower under moderate pressure than the higher one, as in the case of 30°C injection  
387 temperature with 10 MPa injection pressure. On the other hand, higher pressure injection with  
388 higher injection temperature results in faster reservoir cooling and yields rapid decline in the  
389 production temperature, as seen in the scenario 25 MPa injection pressure with 60°C injection  
390 temperature.

391 Similarly, further simulation investigations are carried out by changing only the  
392 injection rate from 10 l/s to 70 l/s under similar lateral well spacing of 0.3 km, by varying the  
393 injection temperatures and pressures as in the previous scenarios. The outcome yields exact  
394 results as in the Fig. 9a, which means that the injection rate has no significance to the simulation  
395 results; this is likely due to the impact of the injection pressure applied to the reservoir.

396 Fig. 9b presents the temperature profile at the production wellhead GPK2 for human-  
397 controlled parameters case two. In this case, the parameters that are kept constant are the lateral  
398 well spacing (0.6 km) and the injection rate (10 l/s) while the injection temperatures and  
399 pressures are varied throughout the simulations. The influence of parameter interaction is  
400 observed to be similar to the previous case, but the production temperature drawdown is more  
401 realistic in comparison to the previous case as shown in Fig. 9a. In the scenario, 30°C injection  
402 temperature with 10 MPa injection pressure, the production wellhead temperature decline is  
403 less than 1% as seen in Fig. 9b. On the other hand, when both the injection temperature and  
404 pressure are increased to 60°C and 25 MPa, respectively, a rapid decline is experienced. The  
405 decline starts just before the simulation reaches ten years, and from then onward, a constant  
406 decline rate is experienced up to the end of the simulation.

407 Likewise, additional experimental simulations are conducted by changing the injection  
408 rate to 70 l/s while all other parameters remain the same, and the results happen to be exactly  
409 as in the previous case.

410

## 411 **5.2 Parameter influence on reservoir cooling**

412 In order to investigate which of the human-controlled parameters is the most influencing in  
413 cooling the reservoir, different scenarios are run with varying injection pressure rate and fluid  
414 injection temperature rate under a constant lateral well distance of 0.6 km, as shown in Fig.  
415 10a-d. As can be seen, the lower the pressure, the less the effect of cooling, whereas with higher  
416 injection pressure rates, the larger the cooling. The low-temperature fluid from the injection  
417 well flows into the extraction well via the fracture; the fluid temperature rises through  
418 convection and conduction from the high-temperature matrix, resulting in superheated fluid in  
419 the extraction well. The significant temperature variation between the injected fluid  
420 temperature (low-temperature) and the matrix temperature (high-temperature) rapidly  
421 decreases the matrix temperature surrounding the injection well. Thus, a relatively low-  
422 temperature area is formed during the initial operation, as seen in Fig. 10a-d. The reservoir  
423 temperature gradually decreases as the exploitation continues, while the low-temperature area  
424 gradually expands. Therefore, it can be concluded that the most influencing parameter  
425 concerning the cooling of the reservoir is the injection pressure rate. To summarise the results  
426 of the above cases, the higher the temperature of the fluid at the injection wellhead when it  
427 interacts with any sufficient injection pressure that can create new hydraulic fractures under a  
428 large well spacing, the lesser the temperature decline at the production wellhead, and vice-  
429 versa.

430 It is observed in Fig. 9a-b and 10a-d that, higher injection pressure causes rapid cooling  
431 of the reservoir. This is because the increase of injection pressure transmits the injected fluid  
432 faster due to more openings in the reservoir and the injected fluid is at relatively low  
433 temperature. Thus, the temperature differences between the reservoir and the injected fluid will  
434 decrease with time due to cooling of the reservoir. The cold water front will propagate in the  
435 reservoir, and it gradually penetrates the production well and causes the decline in the  
436 production temperature with time. In the case of flow rate, the injection flow rate is inversely  
437 proportional to the injection pressure as proven experimentally at the Tianjin geothermal field  
438 in China [35]. In general, as the injection pressure increases, the injection flow rate decreases  
439 and vice-versa.

440

### 441 **5.3 The effect of naturally-occurring parameters on production temperature**

442 In order to examine the effect of different interactions of the naturally-occurring parameters  
443 listed in Table 5 on reservoir productivity, a complete factorial experimental design is  
444 employed, and it rises to 16 distinct operational scenarios are shown in Table 7. The parameters  
445 examined include the geothermal gradient, permeability, thermal conductivity, and porosity.  
446 The results obtained are shown in Fig. 11 and are analysed using four different scenarios. In  
447 the first case, a constant geothermal gradient of 28°C/km and permeability of 1 mD are  
448 employed, while the other two parameters (i.e. thermal conductivity and porosity) are varied  
449 as presented in Fig. 11a. It is clear from Fig. 7a that there is a decline in the production  
450 temperatures in the first two cases, which is due specifically to the lower value of the thermal  
451 conductivities. In the first instance, the decline starts just close to 20 years of simulation, while  
452 in the second case, it just begins after 30 years of simulations. The reason for this difference is  
453 because the porosity in the first scenario is just 10%, while in the second scenario, it is about  
454 40%, as the latter case provides more room for temperature circulation than the former.

455 In the second case, all other parameters remain the same as in the first instance except  
456 the permeability, which is changed from 1 mD to 0.01 mD. Fig. 11b presents the results for the  
457 case, and the maximum temperature obtained at production wellhead GPK2 is approximately  
458 equal to 143°C at about 20 years of simulation. The production temperature begins to decline  
459 in only two cases where the thermal conductivities are very low. The scenario with lower  
460 porosity starts to decrease around 19 years of simulation, while the other with higher porosity  
461 begins at about 31 years of simulation. In cases with higher thermal conductivities, the  
462 production temperatures are stable throughout the simulation period.

463 Similarly, further experimental simulations are carried out by changing the geothermal  
464 gradient from 28°C/km to 38°C/km while all other parameter combinations remain the same  
465 as in the previous two cases. Fig. 11c presents the production temperature profile at wellhead  
466 GPK2 for the instance where the geothermal gradient (38°C/km) and the permeability (1 mD)  
467 are considered at constant rates, and the other parameters (i.e., thermal conductivity and  
468 porosity) are varied throughout the studies. The production temperature curves are similar to  
469 the curves shown in Fig. 11a and b, but the produced temperatures are higher in this case due  
470 to the increase in the geothermal gradient as seen in both Fig. 11c and d.

471 Furthermore, additional numerical simulations are conducted by changing the  
472 permeability to 0.01 mD while all the remaining parameters are the same, and the results appear  
473 to be similar as in the previous case with some little changes in the production temperature  
474 values due specifically to the alterations in the permeability value.

475 The reasons for the increase in the production temperature during the first 20 years of  
476 exploitation are numerous, among which are the geothermal gradient in the reservoir combined  
477 with the effect of significant horizontal distance between the injector and the producer. Also,  
478 the production wellbore being narrower among the reservoir component with lower fluid  
479 temperature before pumping begins, immediately the pumping starts the fluid hotter than that  
480 at the production wellbore is then added to the initial fluid temperature and keeps the  
481 temperature to rise until cooling begins. In this case, the cold water front starts to influence the  
482 produced temperature at approximately 20 years of exploitations.

483 The simulation experimentation results show that the thermal conductivity is the most  
484 influencing parameter regarding the production temperature because of its direct relationship  
485 with permeability, as confirmed by experimental studies; as the permeability increases, the  
486 thermal conductivity rises [36]. The simulation also indicates that porosity has the least effect  
487 concerning the reservoir's productivity, compared to the other parameters. Overall, the  
488 naturally-occurring parameters analysed in this study showed that the parameters contribute  
489 less to reservoir temperature decline because of temperature drawdown, after 60 years of  
490 simulation, of 2°C (for the worst case scenario). It is also evident that heat generation, in this  
491 case, will be more stable. The temperature production requirement proposed has been achieved  
492 in all the 16 scenarios investigated in this case.

493

## 494 **6. Findings and limitations**

495 The sensitivity analysis performed showed that reservoir parameters could be a significant asset  
496 to reservoir engineers/managers during planning, exploration, and exploitation stages. The  
497 parameters analysed are divided into two sets: the first category is referred to as human-  
498 controlled parameters, which are fluid injection temperature, injection pressure rate, injection  
499 rate, and well lateral spacing, whereas the second type is called naturally-occurring parameters  
500 that include permeability, porosity, geothermal gradient, and thermal conductivity.

501 Based on the results obtained in this investigation for naturally-occurring parameters,  
502 it is clear that formation porosity has no significant effect on reservoir productivity regarding  
503 the naturally-occurring parameters. On the other hand, the reservoir permeability, geothermal  
504 gradient, and thermal conductivity have a major impact on reservoir productivity. This study  
505 showed that the permeability and the geothermal gradient of the reservoir are the important  
506 naturally-occurring parameters of the system.

507 For human-controlled parameters, the injection temperature, injection pressure, and  
508 lateral well spacing have the most significant influence on reservoir productivity. Thus, the



509 injection temperature, the injection pressure, and lateral well spacing are critical human-  
510 controlled parameters that can be engineered to obtain the highest temperature production rate.

511 Moreover, the study showed that there is a distinct trend in the variation of the  
512 production temperature with the change of each parameter. Based on the sensitivity analysis  
513 performed, two points are worth noting:

514 (1) The proper knowledge of the geothermal gradient and reservoir permeability are  
515 crucial factors in geothermal energy mining.

516 (2) The injection pressure has to be managed correctly because higher injection rates  
517 affect the reservoir productivity immensely.

518 Thus, the interactions between the parameters investigated in this work should be  
519 considered in relation to their effect on the production temperature and not on the financial  
520 viability or efficiency of the operation. For instance, the porosity does not affect reservoir  
521 productivity, but with respect to drilling operations, the more porous the formation, the less the  
522 operational cost and vice-versa.

523

524

## 525 **7. Conclusions**

526 Based on the geothermal energy plan of the Soultz (France) geothermal field, a 3-D numerical  
527 model has been developed for the lower reservoir (4.5 - 5 km) to examine the long-term  
528 performance of the reservoir using the finite element and factorial experimental design  
529 methods. With the factorial experimental design, various possible combinations of the reservoir  
530 parameters have been found, and their suitability is confirmed by comparing temperature  
531 histories at the production wellbores for the whole scenarios. The human-controlled parameters  
532 happen to have the most unstable temperature distribution at the production wells, and the most  
533 affected parameter regarding that is the fluid injection temperature. On the other hand, the  
534 naturally occurring parameters showed stable temperature distribution at the production wells  
535 in almost all the scenarios. Hence, the results obtained reveal that the reservoir parameters, if  
536 properly managed, can help decision makers maximise reservoir productivity.

537

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542

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- 661

**Table 1:** Model parameters used for the analytical validations [19]

<b>Parameter</b>	<b>Value</b>	<b>Symbol</b>
<b>Spatial discretisation</b>		
Fracture length (m)	50	$L$
Fracture width (m)	2e -3	$b$
Matrix width (m)	63.25	$W$
Increment size x-axis	2	$dx$
Increment size z-axis	0.1265	$dz$
<b>Material properties</b>		
Matrix porosity (%)	1.0	$\phi$
Matrix permeability (m <sup>2</sup> )	1e -15	$\kappa$
Thermal conductivity (W/m/K)	3.0	$\lambda_s$
Solid heat capacity (J/kg/K)	1000	$C_{\rho,S}$
Fluid heat capacity (J/kg/K)	4000	$C_{\rho,L}$
Solid density (kg/m <sup>3</sup> )	2600	$\rho_s$
Fluid density (kg/m <sup>3</sup> )	1000	$\rho_L$
<b>Initial conditions</b>		
Pressure (Pa)	1e +5	$P_{in}$
Temperature (°C)	0	$T_{in}$
<b>Boundary conditions</b>		
Injection Temperature (°C)	1.0	$T_{inj}$
Inlet velocity (m/s)	1e -3	$v$
Production pressure	1e +5	$P_{pro}$

**Table 2:** Percentage difference between measured and simulated temperature profile at GPK2

<b>Vertical depth (m)</b>	<b>Measured temperature (°C)</b>	<b>Simulated temperature (°C)</b>	<b>Percentage difference (%)</b>
-3570	149	147	1.35
-3730	159	154	3.19
-4030	168	165	1.80
-4400	179	179	0.00
-4760	191	193	1.04
-5140	202	207	2.44

**Table 3:** Physical properties attributed to lower reservoir (less permeable granitic basement)  
[15], [32], [33]

<b>Parameter</b>	<b>Value</b>	<b>Symbol</b>
<b>Matrix</b>		
Porosity (%)	1.0	$\phi$
Permeability (mD)	0.001	$\kappa$
Thermal conductivity (W/m/K)	3.0	$\lambda_s$
Heat capacity (J/kg/K)	850	$C_{\rho,s}$
Density (kg/m <sup>3</sup> )	2600	$\rho_s$
<b>Fracture</b>		
Porosity (%)	0.1	$\phi_f$
Permeability (mD)	10	$\kappa_f$
Thermal conductivity (W/m/K)	2.5	$\lambda_f$
Heat capacity (J/kg/K)	750	$C_{\rho,f}$
Density (kg/m <sup>3</sup> )	2000	$\rho_f$



**Table 4:** Range of values for the human-controlled parameters used in the reservoir model

<b>Parameter</b>	<b>Minimum Value (-)</b>	<b>Maximum Value (+)</b>
Injection rate (l/s)	10	70
Lateral well spacing (km)	0.3	0.6
Injection temperature (°C)	30	60
Injection pressure (MPa)	10	25

**Table 5:** Range of values for the naturally-occurring parameters used in the reservoir model

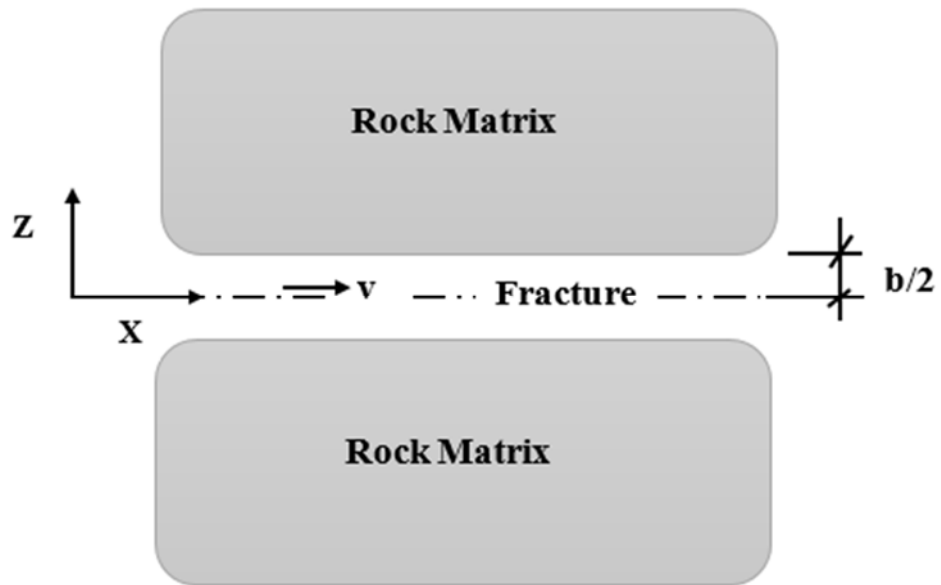
<b>Parameter</b>	<b>Minimum Value (-)</b>	<b>Maximum Value (+)</b>
Geothermal gradient (°C/km)	28	38
Permeability (mD)	1.0	0.01
Thermal conductivity (W/m/K)	1.0	3.5
Porosity (%)	10	40

**Table 6:** Human-controlled parameter combinations

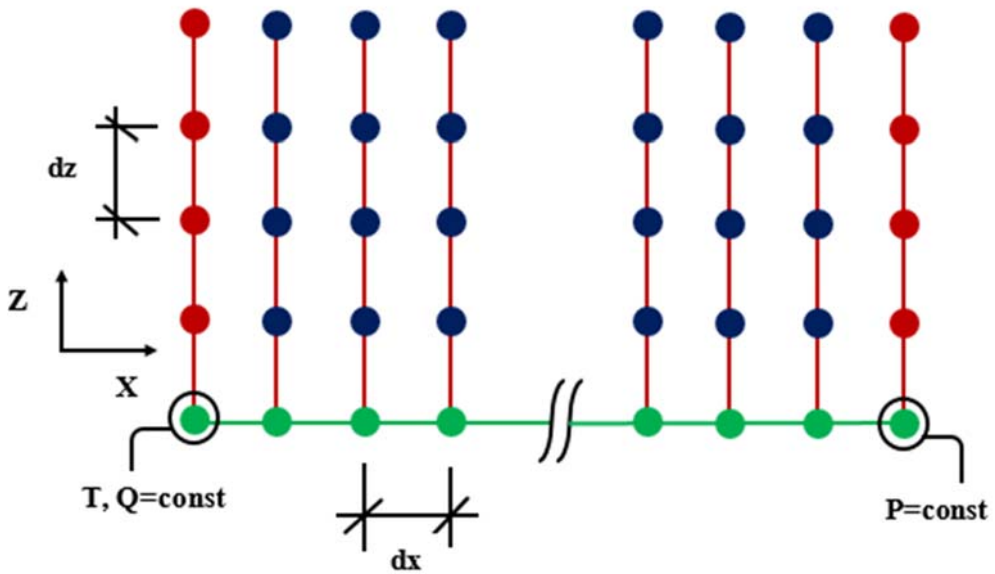
<b>Run number</b>	<b>Lateral well spacing (km)</b>	<b>Injection rate (l/s)</b>	<b>Injection temperature (°C)</b>	<b>Injection pressure (MPa)</b>
1	0.3	10	30	10
2	0.3	10	30	25
3	0.3	10	60	10
4	0.3	10	60	25
5	0.3	70	30	10
6	0.3	70	30	25
7	0.3	70	60	10
8	0.6	70	60	25
9	0.6	10	30	10
10	0.6	10	30	25
11	0.6	10	60	10
12	0.6	10	60	25
13	0.6	70	30	10
14	0.6	70	30	25
15	0.6	70	60	10
16	0.6	70	60	25

**Table 7:** Naturally-occurring parameter combinations

<b>Run number`</b>	<b>Geothermal gradient (°C/km)</b>	<b>Permeability (mD)</b>	<b>Thermal conductivity (W/m/K)</b>	<b>Porosity (%)</b>
1	28	0.01	1.0	10
2	28	0.01	1.0	40
3	28	0.01	3.5	10
4	28	0.01	3.5	40
5	28	0.01	1.0	10
6	28	0.01	1.0	40
7	28	0.01	3.5	10
8	28	0.01	3.5	40
9	38	1.0	1.0	10
10	38	1.0	1.0	40
11	38	1.0	3.5	10
12	38	1.0	3.5	40
13	38	1.0	1.0	10
14	38	1.0	1.0	40
15	38	1.0	3.5	10
16	38	1.0	3.5	40



**Fig. 1:** Model geometry for the fracture-matrix heat transport (Adopted [19])



**Fig. 2:** Grid alignment and boundary conditions for the numerical model

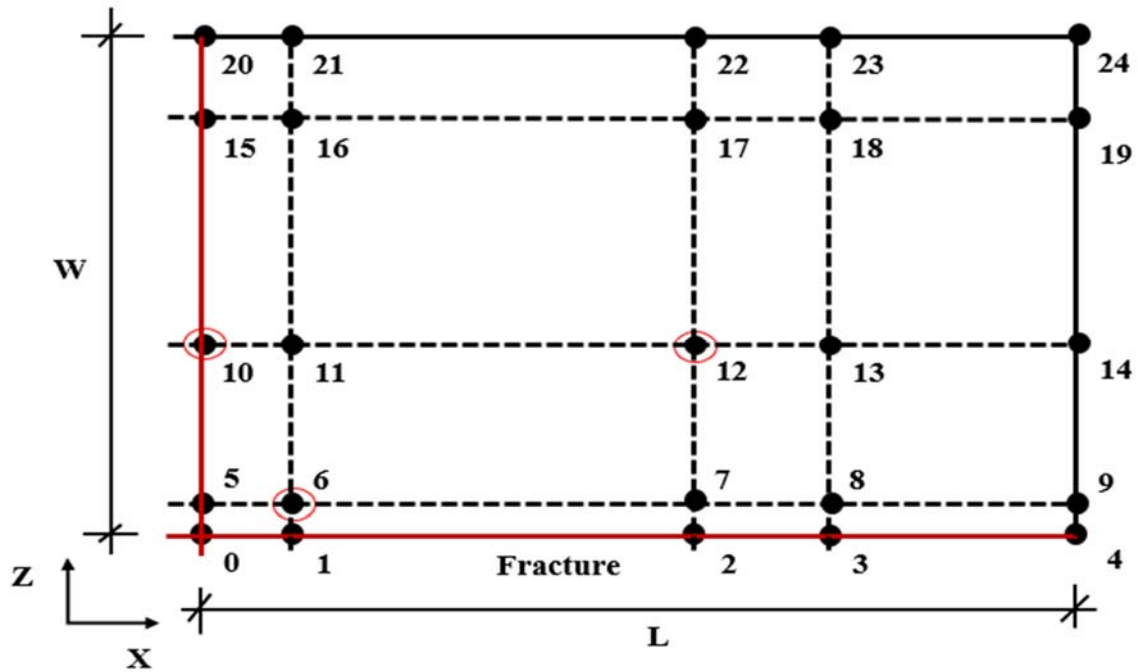


Fig. 3: Observation points positions (i.e., 6, 10, and 12) for temperature history curves

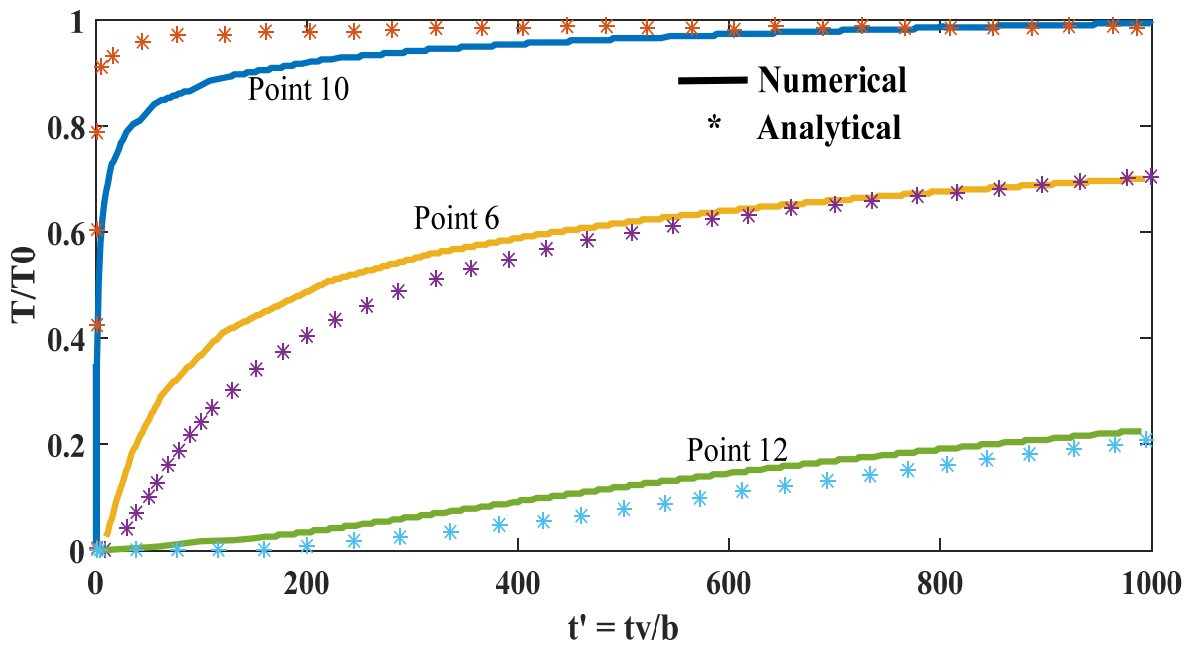
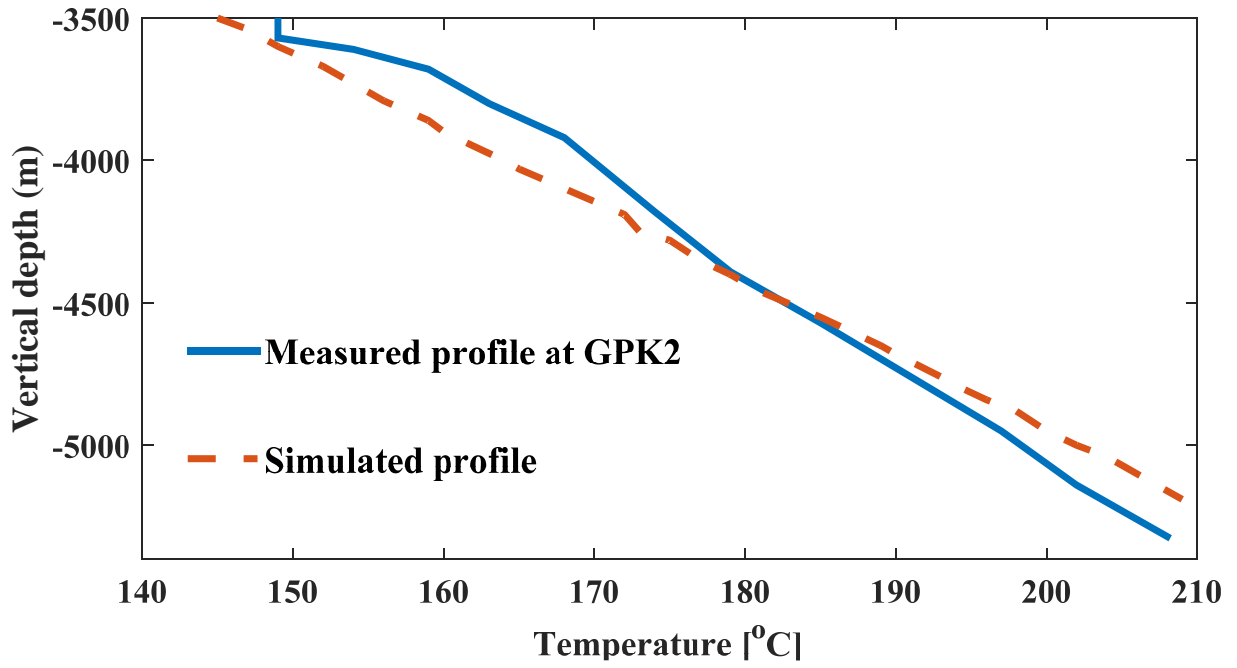
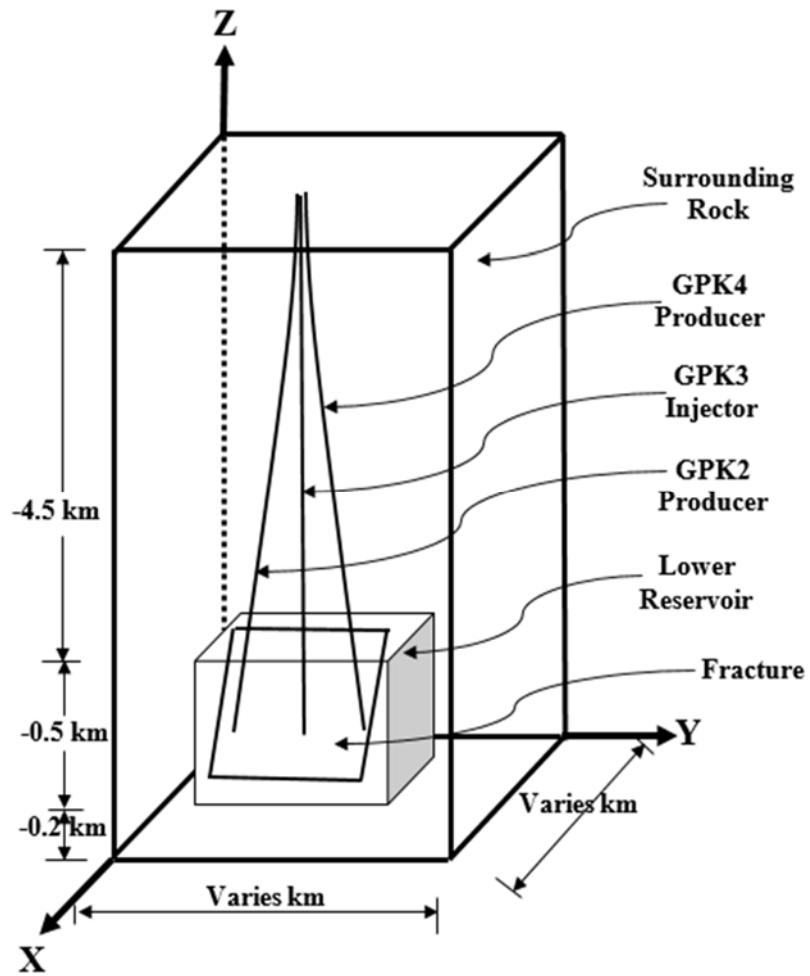


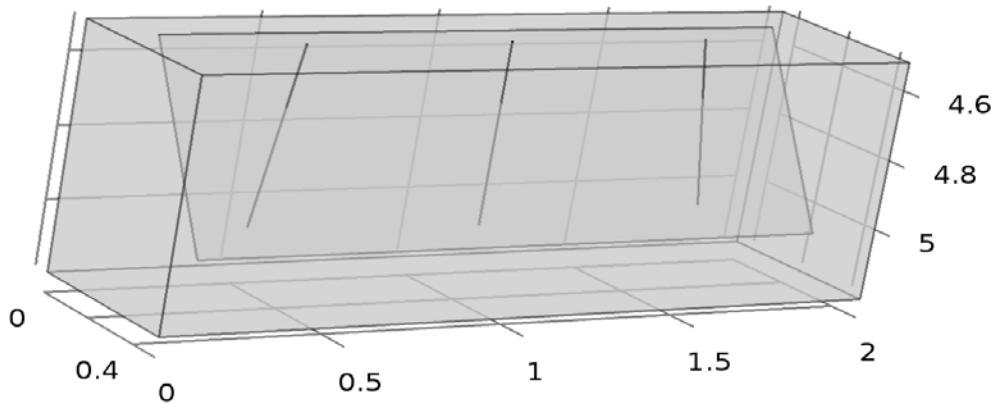
Fig. 4: Temperature history curves at certain locations in the rock matrix for both the analytical and numerical models



**Fig. 5:** Temperature profile at GPK2 well compared with simulated profile

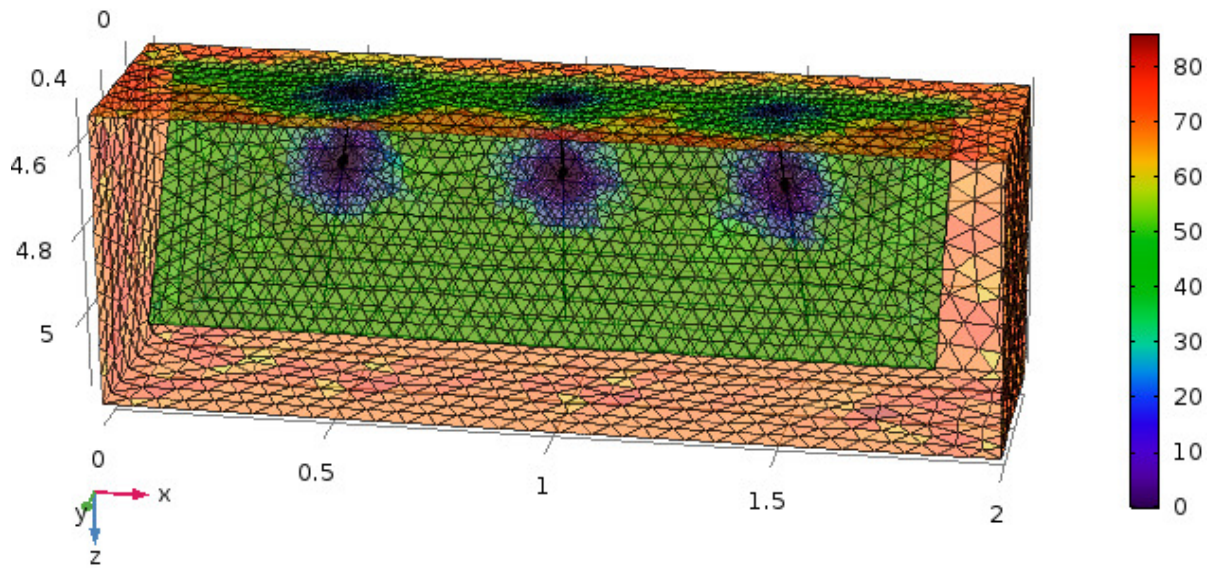


**Fig. 6:** Schematic representation of the Soultz geothermal system

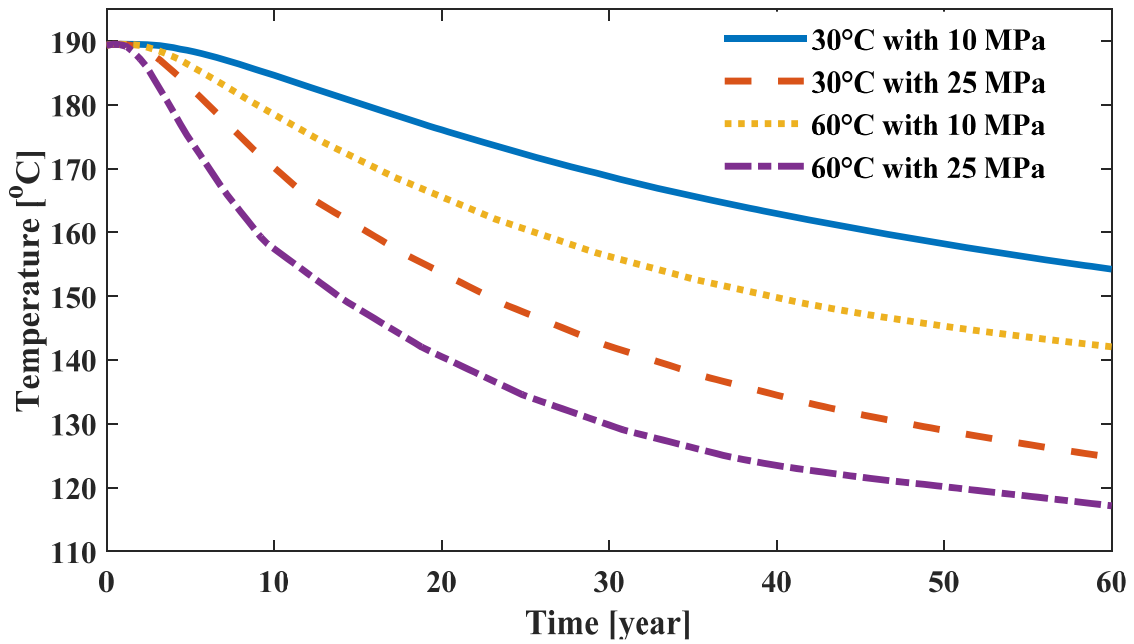


**Fig. 7:** Lower reservoir geometry (km)

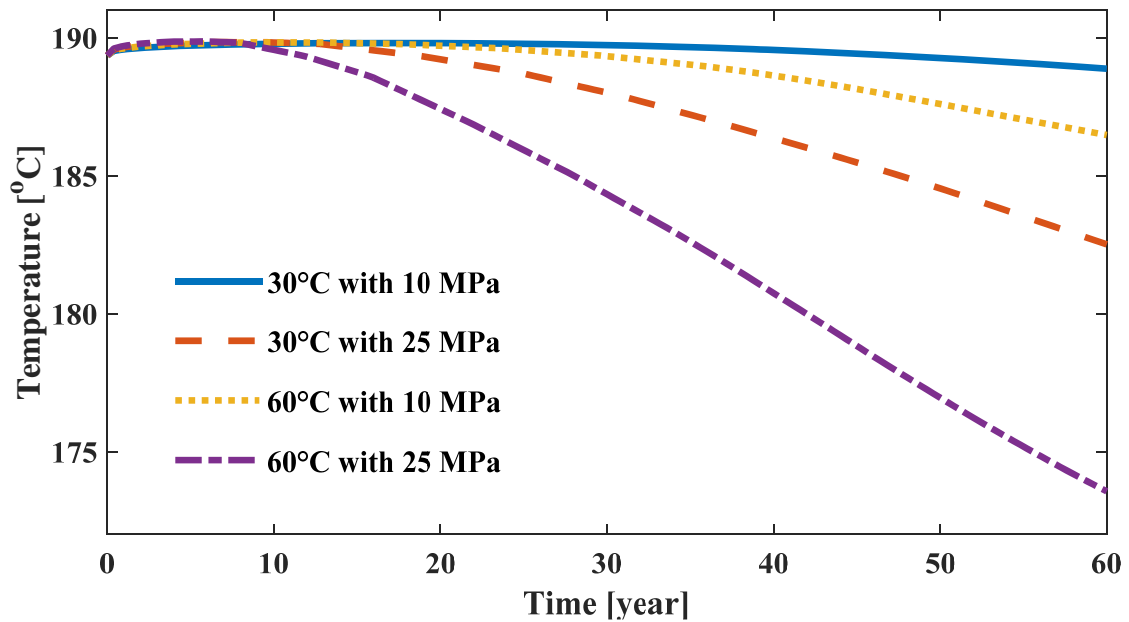




**Fig. 8:** Lower reservoir mesh element sizes and distributions (m)

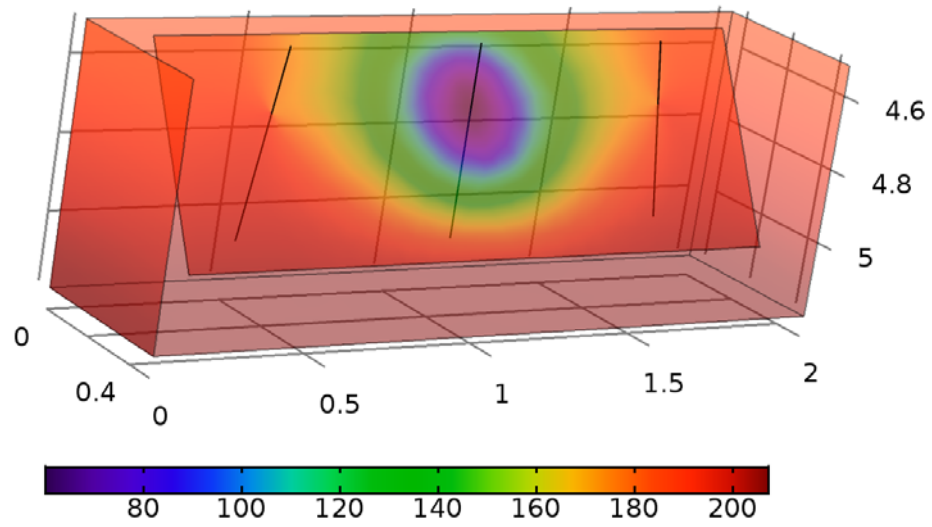


**Fig. 9a:** Production temperature at wellhead GPK2 with constant injection rate 10 l/s and 0.3 km lateral well spacing under the influence of various injection temperatures and pressures

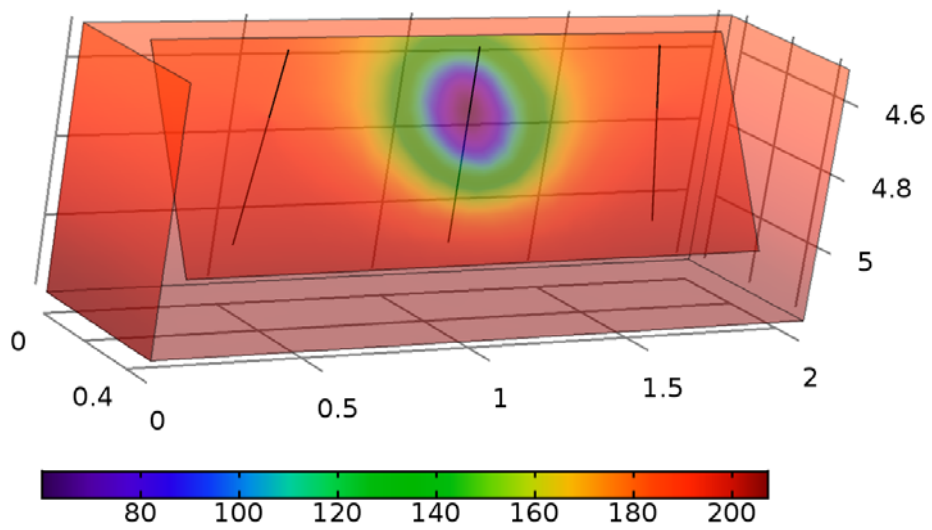


**Fig. 9b:** Production temperature at wellhead GPK2 with constant injection rate 10 l/s and 0.6 km lateral well spacing under the influence of various injection temperatures and pressures

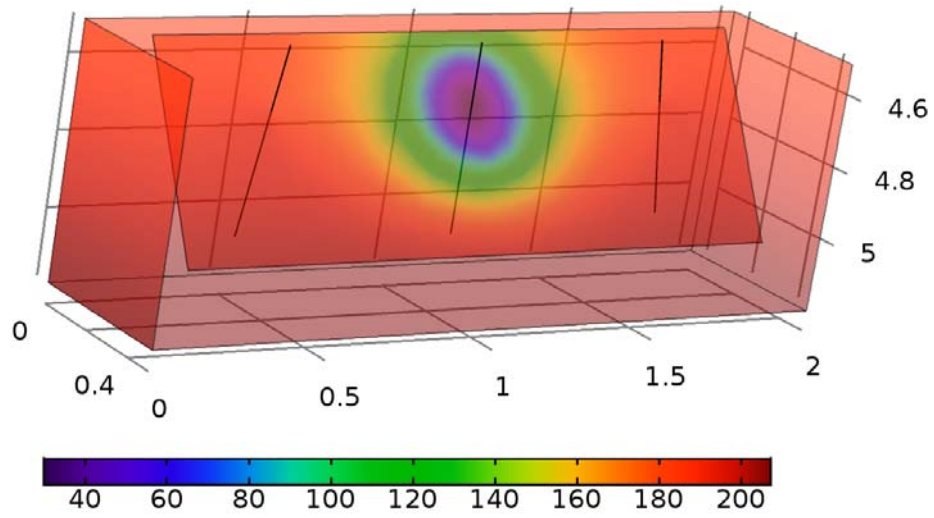
**Fig. 9:** Production temperature at wellhead GPK2 for human controlled parameters under the influence of multiple parameter interaction



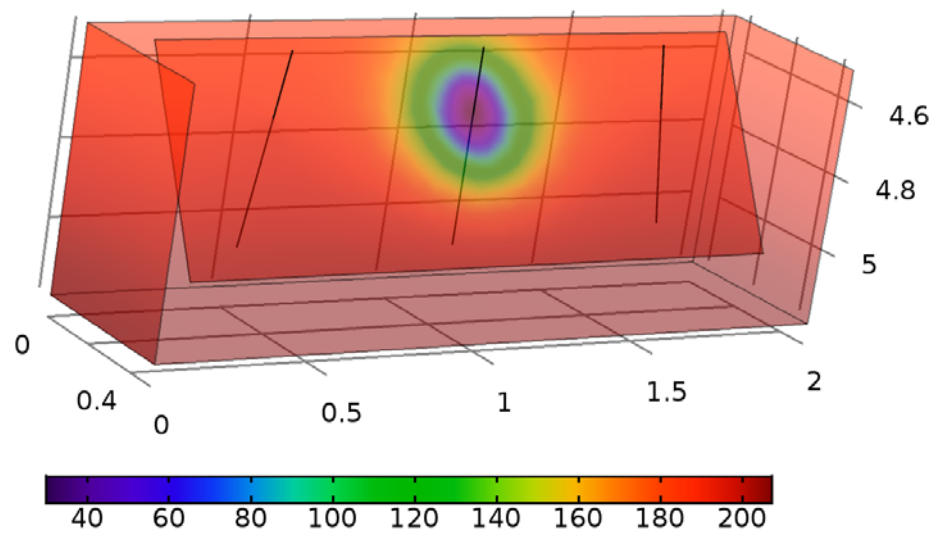
**Fig. 10a:** Reservoir cooling ( $^{\circ}\text{C}$ ) under the effect of  $60^{\circ}\text{C}$  fluid injection temperature with 25 MPa injection pressure rate



**Fig. 10b:** Reservoir cooling ( $^{\circ}\text{C}$ ) under the effect of  $60^{\circ}\text{C}$  fluid injection temperature with 10 MPa injection pressure rate

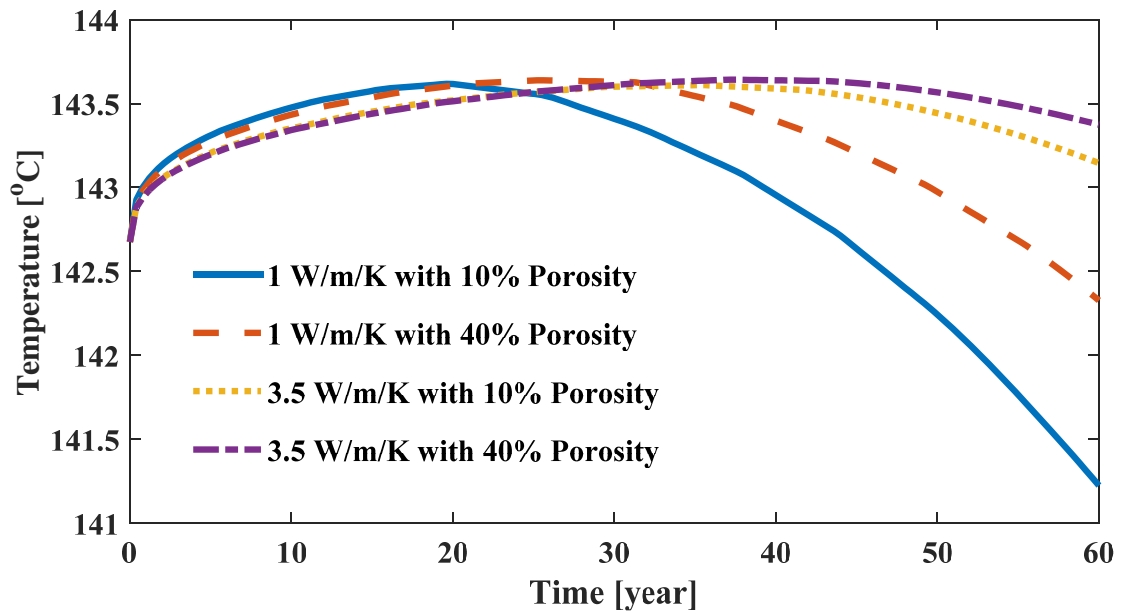


**Fig. 10c:** Reservoir cooling (°C) under the effect of 30°C fluid injection temperature with 25 MPa injection pressure rate

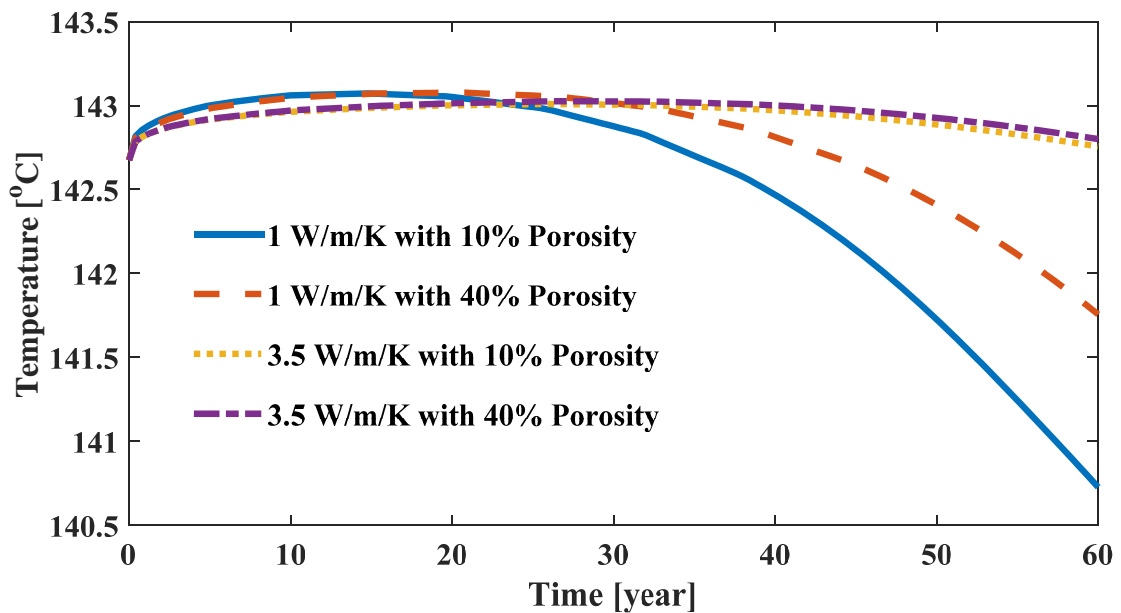


**Fig. 10d:** Reservoir cooling (°C) under the effect of 30°C fluid injection temperature with 10 MPa injection pressure rate

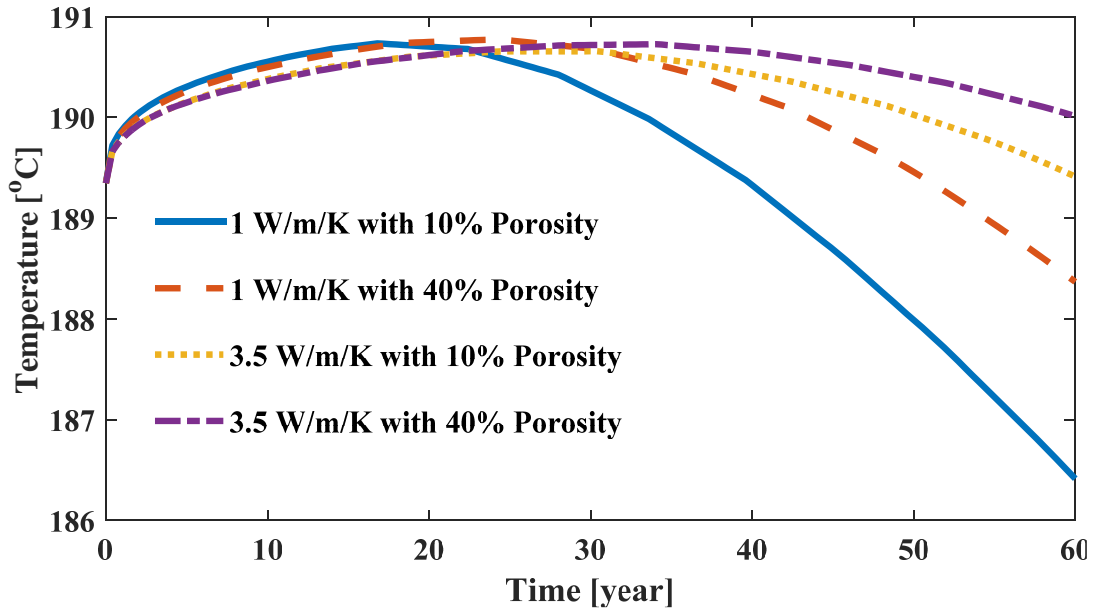
**Figure 10:** Reservoir cooling (°C) as a function of fluid injection temperature and pressure rate after 60 years of simulation



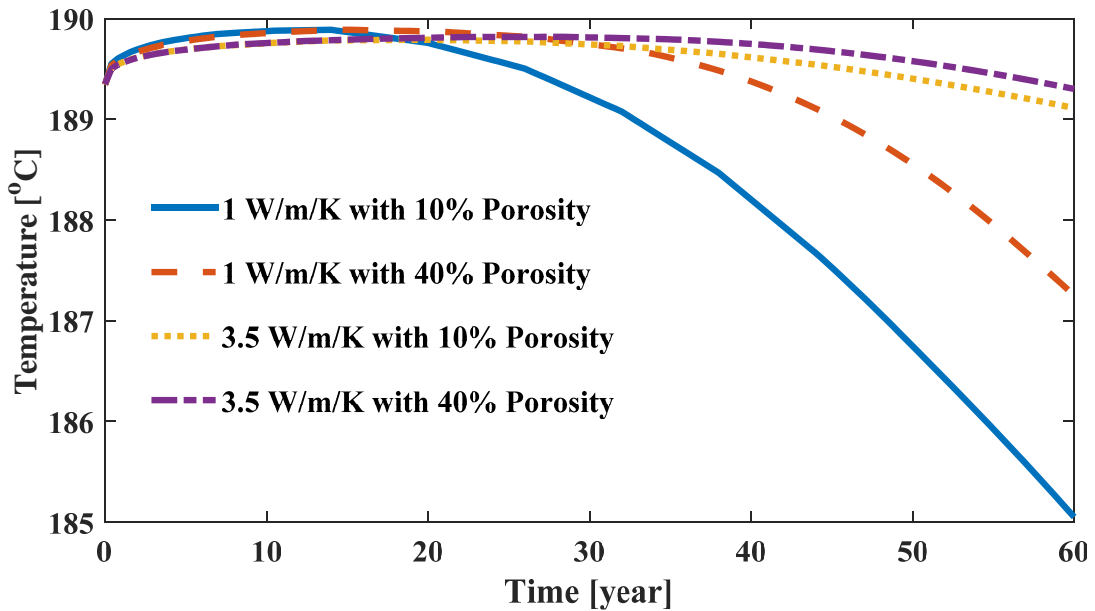
**Fig. 11a:** Production temperature at wellhead GPK2 with constant geothermal gradient 28°C/km and 1 mD permeability under the influence of various thermal conductivities and porosities



**Fig. 11b:** Production temperature at wellhead GPK2 with constant geothermal gradient 28°C/km and 0.01 mD permeability under the influence of various thermal conductivities and porosities



**Fig. 11c:** Production temperature at wellhead GPK2 with constant geothermal gradient  $38^{\circ}\text{C}/\text{km}$  and  $1\text{ mD}$  permeability under the influence of various thermal conductivities and porosities



**Fig. 11d:** Production temperature at wellhead GPK2 with constant geothermal gradient  $38^{\circ}\text{C}/\text{km}$  and  $0.01\text{ mD}$  permeability under the influence of various thermal conductivities and porosities

**Fig. 11:** Production temperature at wellhead GPK2 for naturally occurring parameters under the influence of multiple parameter interaction